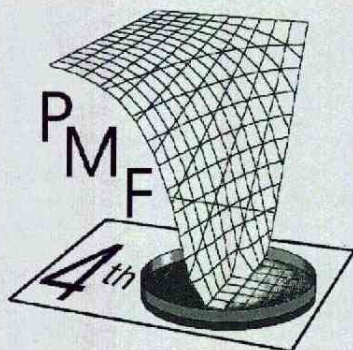


June 15•19, 2003 Quimper•France  
15•19 Juin 2003

**Predictive**  
*modélisation*  
**modelling**  
*prévisionnelle*  
**in foods**  
*dans les aliments*

4<sup>th</sup> International  
Conference



Conference Proceedings

Editors : J.F.M. Van Impe, A.H. Geeraerd, I. Leguérinel and P. Mafart

With support of the Société Française de Microbiologie  
*Avec le parrainage de la Société Française de Microbiologie*



ISBN 90-5682-400-7

**Development of a tool in order to simulate the behaviour of pathogens and evaluate the incidence of technological choices in ready-prepared fresh or pasteurised vegetable foodstuffs**

L. Coroller<sup>1</sup>, C. Denis<sup>2</sup>, V. Stahl<sup>3</sup> and D. Thuault<sup>1</sup>

<sup>1</sup> ADRIA, ZA Creac'h Gwen, 29196 Quimper Cedex, France

<sup>2</sup> ADRIA NORMANDIE, bd 13 juin 1944, 14 310 Villers Bocage, France

<sup>3</sup> Aérial, 19 rue de ST Junien BP23, 67305 Schiltigheim, France .....268

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<sup>1</sup> NIZO food research, Department of Processing, Quality & Control, PO Box 20, 6710 BA Ede, The Netherlands

<sup>2</sup> Honeywell, Department of Industrial Automation & Control, Laarderhoogtweg 18, 1101 EA Amsterdam, The Netherlands .....271

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<sup>1</sup> Flanders Centre/Laboratory of Postharvest Technology, W. de Croylaan 42, B-3001 Leuven, Belgium

<sup>2</sup> BioTeC – Bioprocess Technology and Control, Department of Chemical Engineering, Katholieke Universiteit Leuven, W. de Croylaan 46, B-3001 Leuven, Belgium

<sup>3</sup> Laboratory for Food Microbiology, Katholieke Universiteit Leuven, Kasteelpark Arenberg 23, B-3001 Leuven, Belgium .....274

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<sup>1</sup> National Food Administration, P.O. Box 622, SE-751 26 Uppsala, Sweden

<sup>2</sup> Swedish University of Agricultural Sciences, Dep. of Microbiology, P.O. Box 7070, SE 750 07 Uppsala, Sweden .....280

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J.P. Sutherland<sup>1</sup>, V.D. Prajapat<sup>1</sup> and P. Braun<sup>2</sup>

<sup>1</sup> Food Microbiology Unit, Department of Health and Human Sciences, London Metropolitan University, 166-220 Holloway Road, London N7 8DB, UK

<sup>2</sup> Institut für Lebensmittelhygiene, University of Leipzig, An den Tierkliniken 1, D - 04103 Leipzig, Germany.....283

**Cooling of pig carcasses**

G. Szabó<sup>1</sup>, R. Rajkó<sup>1</sup> and F. Eszes<sup>2</sup>

<sup>1</sup> Department of Food Engineering and Environmental Techniques University of Szeged, Mars ter 7., Hungary

<sup>2</sup> Department of Food Technology and Environmental Management of the University of Szeged, Mars ter 7., Hungary .....286

## Cooling of pig carcasses

G. Szabó<sup>1</sup>, R. Rajkó<sup>2</sup>, F. Eszes<sup>3</sup>

<sup>1,2</sup>Department of Food Engineering and Environmental Techniques University of Szeged, Mars ter 7.,  
<sup>1</sup>(szabo.g@bibl.szef.u-szeged.hu) <sup>2</sup>(rajko@sol.u-szeged.hu)

<sup>3</sup>Department of Food Technology and Environmental Management of the University of Szeged, Mars ter 7.,  
Hungary, (feri@bibl.szef.u-szeged.hu)

### Introduction

The fulfilling of the new food safety prescriptions is not an easy task because we had to reach the core temperature within 2 hours. Therefore new temperature programs have been offered recently. This are under  $-20^{\circ}\text{C}$ . It is advantageous in the bacteriological point of view but the risk of the cold shortening and appearing ice crystals increase if we do not break this process in the right time. The resulting very high speed of cooling slow down the biochemical and rigor mortis processes, which is not good either for meat processing or meat trade as well.

Our aim was to investigate whether the new prescription of  $7^{\circ}\text{C}$  temperature in the carcass how can be achieved the new temperature programmes avoiding both the deterioration and cold shortening. in small scale slaughterhouses.

### Material and methods

The cold shortening limit temperature was chosen to  $12^{\circ}\text{C}$  till 12 hours and the deterioration limit  $20^{\circ}\text{C}$  within 10 hours according to Rosset (1982). We used the equation for 1 dimensional body

$$\frac{T - T_a}{T_0 - T_a} = \sum_{n=1}^{\infty} \frac{\sin(\beta_n)}{2\beta_n + \sin(2\beta_n)} e^{-\beta_n^2 Fo} \cos\left(\beta_n \frac{x}{X}\right) \quad (1)$$

where  $T$  = measured temperature at a point [ $^{\circ}\text{C}$ ]

$T_a$  = ambient temperature [ $^{\circ}\text{C}$ ]

$T_0$  = Initial temperature [ $^{\circ}\text{C}$ ]

$\beta$  = First root of the characteristic equation  $\beta \text{tg}(\beta) = \text{Bi}$

$\text{Bi} = \alpha X / \lambda$

$\alpha$  = Surface heat transfer coefficient [ $\text{W}/\text{m}^2\text{K}$ ]

$\lambda$  = Thermal conductivity of the carcass meat [ $\text{W}/\text{mK}$ ]

$X$  = characteristic length [m]

$Fo = \alpha t / X$

The calculation was made for leg.. The characteristic length are calculated by equation 4 (Prändtl 1988)

$$X = 0,075 \left( 1 + \frac{M}{100} \right) \quad (2)$$

where  $X$  = characteristic length [m]

$M$  = carcass weight [kg]

The surface heat transfer coefficients were finite and assumed from 5 to  $100 \text{ W}/\text{m}^2\text{K}$  (from free convection to very strong convection at the blowing in) The initial temperature was  $40^{\circ}\text{C}$ . The bacteriological count was calculated by the method of Dantigny (1999) for *E. coli*. with an initial concentration of  $10^4/\text{cm}^2$

## Results

First we investigated whether the one phase cooling can be applied for the new 7°Cwitin 24 hours prescription. Without deterioration and cold shortening.

Table 1: Time to reach 7°C in core and cooling temperature and surface heat transfer coefficient

Cooling temperature [°C]	Surface heat transfer coefficient [W/m <sup>2</sup> K]	Cooling time [hours]
0	15-30	21-16,5
-5	10-20	20-16,5
-15	10	16,5

In the Table 1 we show only the parameters fulfilling the no deterioration and no cold shortening conditions. We can see that the surface heat transfer coefficient has to be lowered to avoid cold shortening if we lower the cooling temperature. About 10 W/m<sup>2</sup>K surface heat transfer coefficient change is equal to a change caused by 5°C cooling temperature change relating to the cooling time. The lowering of the cooling temperature affect the surface temperature and the bacterial count on the surface as well (Figure 1).

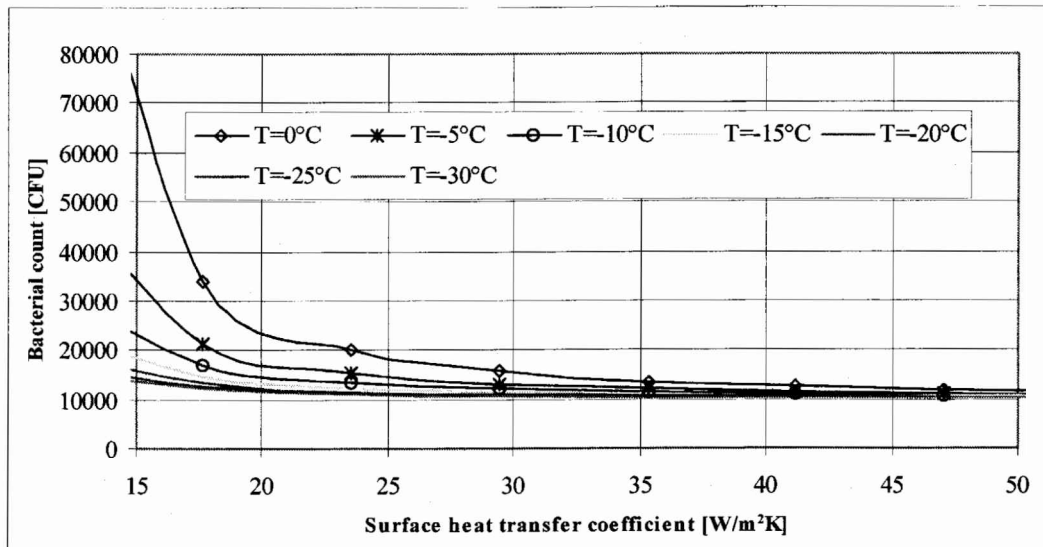


Figure 1: Bacterial count development at the surface at different surface heat transfer coefficient and cooling temperature

From figure 1 we can see that the surface bacterial count can be lowered significantly if we change the ambient temperature from 0°C to -10 centigrade. After that the differences became lower and lower between the cooling temperatures and seems to be a maximum useful surface heat transfer coefficients of 40W/m<sup>2</sup>K. If we would have chosen lower initial CFU count we could have the same picture but lower CFU of course.

If we consider a two phase cooling as proposed by Klettner (1996) we have to investigate when we reach the 0°C because we do not want to freeze the carcass.(Figure 2). We can see from the figure 2 that the freezing region can be achieved more quickly if we apply lower temperature but it is not worthy to go under -15°C because we win only very few amount of time. An another aspect of this figure that the exposition time at the lowest temperature is so short that only the surface temperature lowered but the cooling time is not significantly less and will be very similar to the one phase cooling with a temperature of 0÷-5°C.

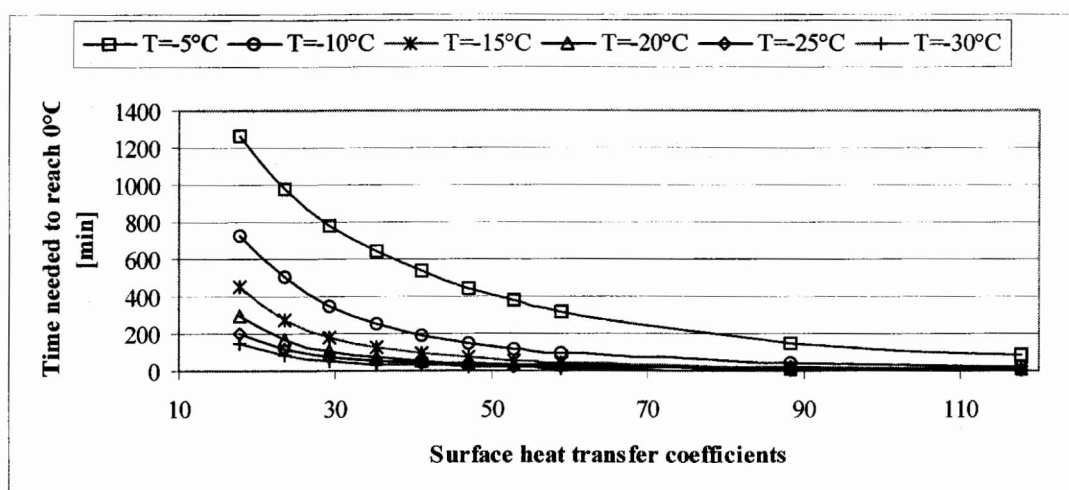


Figure 2: Time to reach 0°C in the surface [min]

## Conclusions

The small plants can use the older cooling system if they have enough reserve in it because we do not need to lower the cooling temperature under  $-15^{\circ}\text{C}$  (preferably  $-10^{\circ}\text{C}$ ). Under this temperature we get no advantage both in cooling time and in bacterial count.

In case of very low cooling temperature there is a very short effective time for cooling at low temperature and we approximate the in the second part of cooling the constant temperature cooling of  $0^{\circ}\text{C}$  to  $-5^{\circ}\text{C}$ .

The limit surface heat transfer coefficient is about  $30\text{--}40\text{W/m}^2\text{K}$ , which means not more than  $5\text{ m/s}$  in air velocity. In the practice the problem is that this  $5\text{--}10\text{m/s}$  can be measured only at blowing in area meanwhile a little distance from it can be measured  $0,5\text{--}2\text{ m/s}$ . It means that if we would like to have a  $4\text{--}5\text{m/s}$  among the carcasses we need to blow in the air with a velocity more than  $10\text{m/s}$ .

This is not usual in the mechanical engineering recommendations for closed spaces because of the high pressure drop and increase of the ventilator power consumption. We recommend therefore an air manifold system directing their blow out openings on to the leg of the carcasses. It would mean a  $7.2\text{ m}^3/\text{h}$  in case of  $40\text{ mm}$  diameter and pro carcasses.

## Acknowledgements

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