



Sonochemical Deposition of Palladium Nanoparticles Onto the Surface of N-Doped Carbon Nanotubes: A Simplified One-Step Catalyst Production Method

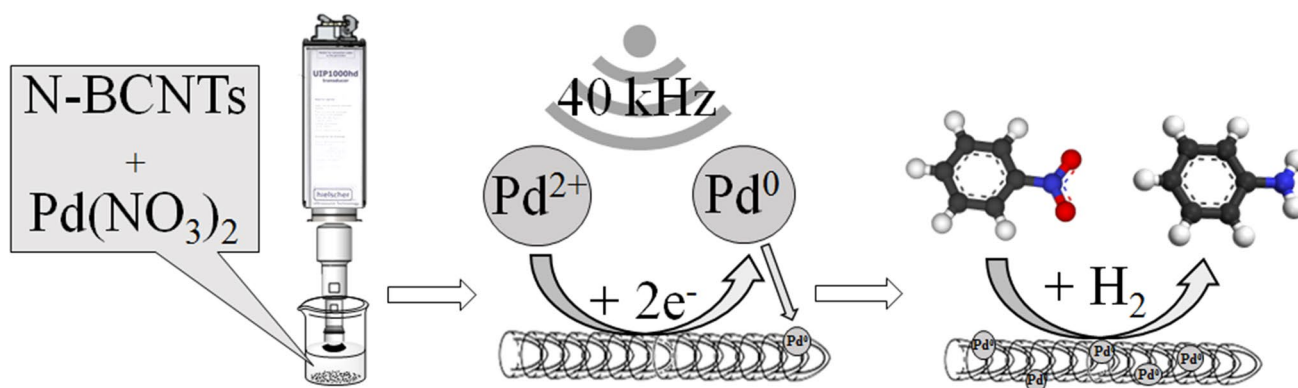
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Abstract

This work presents an easy, one-step procedure for catalyst preparation. A small fraction of palladium ions was reduced to Pd nanoparticles and deposited onto the surface of nitrogen-doped carbon nanotubes (N-BCNT) by acoustic cavitation using high-intensity ultrasound in aqueous phase, where N-BCNT served as a reducing agent. The formation of elemental palladium and palladium oxides were confirmed and the particle size is < 5 nm. The catalytic activity of the synthesized Pd/N-BCNT catalyst was tested in nitrobenzene hydrogenation at four different temperature (273–323 K) and 20 bar pressure. The catalyst showed high activity despite the presence of palladium oxide forms, the conversion of nitrobenzene to aniline was 98% at 323 K temperature after 40 min. The activation energy was 35.81 kJ/mol. At 303 K and 323 K temperature, *N*-methylaniline was formed as by-product in a small quantity (8 mmol/dm³). By decreasing the reaction temperature (at 273 K and 283 K), the reaction rate was also lower, but it was favourable for aniline selectivity, and not formed *n*-methylaniline. All in all, Pd/N-BCNT catalyst was successfully produced by using a one-step sonochemical method, where further activation was not necessary as the catalytic system was applicable in nitrobenzene hydrogenation.

Graphic Abstract



Keywords Ultrasound · N-CNT · Nitrobenzene · Hydrogenation

1 Introduction

Aniline is a versatile organic compound intensively used in the chemical industry, and mainly applied in the production of polyurethane precursors. Several different procedures have been developed to synthesize aniline such as

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nitrobenzene reduction by iron in the presence of hydrochloric acid (Béchamp process) [1], phenol amination [2], and nitrobenzene hydrogenation [3–5]. The industrial production of aniline includes the latter, nitrobenzene hydrogenation, where a wide variety of catalysts can be used. Usually, the catalyst consists of a catalytically active metal (e.g. Ni, Pd, Pt, Cu) and a carrier or support (e.g. various carbon forms, alumina, silica, zeolites). Pd, Pt, Ru, and Rh decorated catalysts with carbon (C), silica (SiO₂) or alumina (Al₂O₃) supports were compared in aniline synthesis [6]. The catalytic activity varied depending on the applied metal (Pt > Pd > Ru, Rh), and carriers (C > Al₂O₃, SiO₂). Nanostructured carbon forms, mainly carbon nanotubes (CNTs) are the most widely applied and studied support materials, owing to their fascinating properties such as, extraordinary mechanical strength, good chemical stability and large surface area [7]. CNTs do not have micropores, thus, there is no mass transfer limitation during the catalytic processes which leads to higher reaction rates and better efficiency. Several studies have shown that a wide range of reactions including sorbitol hydrogenolysis to glycols, nitrocyclohexene hydrogenation, CO₂ reduction, Fischer–Tropsch and aniline synthesis can be successfully catalysed by using CNT-based catalysts with different metals (Pd, Pt, Ru, Ni) [6, 8–17]. The characteristics of carbon nanotubes can be further fine-tuned by incorporating heteroatoms into their structure [18]. Such incorporation can be done by using nitrogen containing carbon compounds as starting materials for the synthesis of CNTs, which will induce the formation of nitrogen-doped bamboo-like carbon nanotubes (N-BCNT) [19]. N-BCNTs have more defect sites than their single- or multi-walled counterparts, and due to the incorporated nitrogen atoms, they also have special adsorption points which are excellent spots for catalytically active metal particles [20, 21].

In several cases, the catalyst preparation procedures included an activation step, within which the metal-ions, -oxides and -complex ions were reduced by hydrogen gas to a catalytically active form, a metallic phase. However, the activation step is time and energy consuming. A viable alternative for metal nanoparticle production is applying acoustic cavitation. By using high-intensity ultrasound treatment, the formation of vapour microbubbles can be induced in metal ion solutions. Then, these bubbles will collapse and this leads to intense local heating (~ 5000 K), high pressure (~ 1000 atm), enormous heating and cooling rates (> 109 K/s) and liquid jet streams (~ 400 km/h) within small volumes, which are the so-called “hot spots” [22]. The energy in the “hot spots” can cover the needs of chemical reactions such as the reduction of metal ions to metals (e.g. Au, Co, Fe, Pd, Ni, Au/Pd and Fe/Co) in the presence of a reducing agent [23–28]. In our work, a one-step sonochemical catalyst preparation method is developed which does not require any post-treatment in order to activate the

catalyst. The reducing agent in this redox process is the catalyst support itself, which is N-BCNT in this case, and it is oxidized during the reduction of the Pd²⁺ ions. The overall procedure will lead to the deposition of elemental palladium, palladium(II) oxide and palladium(IV) oxide particles onto the surface of the N-BCNT support.

2 Materials and Methods

N-BCNT synthesis was carried out by using a CCVD method [19]. To achieve the catalytic system, the synthesized N-BCNT supports were decorated with palladium starting from palladium (II) nitrate dihydrate (Pd(NO₃)₂·2H₂O, Merck). Palladium nitrate dihydrate as Pd precursor (0.20 g) was solved in 1000 ml distilled water, and 1.00 g N-BCNT was added to the solution. The aqueous dispersion was sonicated by a Hielscher Ultrasound tip (UIP1000 HdT) homogenizer (78 W) for 10 min. After the sonication and an additional 30 min contact time, the dispersion was filtered, and the Pd contained nanotubes were dried at 120 °C overnight.

The final palladium nanocomposite catalyst was tested in nitrobenzene (Sigma Aldrich) hydrogenation. To identify the products analytical standards (Dr. Ehrenstorfer) such as aniline, nitrobenzene, nitrosobenzene and *N*-methylaniline were used.

The catalyst was examined (morphology, particle size and structure of the palladium nanoparticles) by high-resolution transmission electron microscopy (HRTEM, FEI Technai G2 electron microscope, 200 kV). The specimens were prepared by dropping aqueous suspension of the samples on 300 mesh copper grids (Ted Pella Inc.).

X-ray diffraction (XRD) measurements were carried out by Bruker D8 Advance diffractometer (Cu-K α source, 40 kV and 40 mA) in parallel beam geometry (Göbel mirror) with Vantec1 detector to identify and quantify the crystalline phases of the palladium.

Functional groups on the surface of the nanotube support were studied by using Fourier-transform infrared spectroscopy (FTIR, Bruker Vertex 70 spectrometer).

The incorporated nitrogen forms and the oxidation states of the palladium were studied by X-ray photoelectron spectroscopy with a SPECS instrument applying equipped with a Phoibous 150 MCD nine analyser. The Al K α x-ray source was operated at 14 kV and 10.8 mA (150 W). The analyser was operated FAT mode with a pass energy of 20 eV. High resolution spectra were acquired by averaging of 15 spectra of each region. CasaXPS software was used for data evaluation. The binding scale was set so that the adventitious carbon C1s peak is at 284.8 eV.

The hydrogenation of nitrobenzene was carried out in a Büchi Uster Picoclave reactor system. The pressure of hydrogenation was 20 bar, the reaction temperature was set to

283 K, 293 K, 303 K and 313 K, while the rotational speed was 1000 rpm. Sampling took place after the beginning of the reaction at 0, 5, 10, 15, 20, 30, 40, 60, 80, 120, 180, and 240 min. The hydrogenation process was followed by Agilent 7890A gas chromatograph coupled with Agilent 5975C Mass Selective detector. The separation was performed on a RTX-624 column (60 m × 0.25 mm × 1.4 μm). The injected sample volume was 1 μL at 200:1 split ratio, while the inlet temperature was set to 473 K. The carrier gas was helium with constant flow (2.28 mL/min), and the oven temperature was set to 323 K for 3 min and it was heated up to 523 K with 10 K/min increments and kept there for another 3 min.

The efficiency of the catalytic hydrogenation was studied by calculating the conversion, X% of nitrobenzene based on the following equation (Eq. 1):

$$X\% = \frac{\text{consumed } n_{\text{nitrobenzene}}}{\text{initial } n_{\text{nitrobenzene}}} \times 100 \quad (1)$$

By assuming that the process is a first-order reaction [29–31]. Based on the initial and measured nitrobenzene concentrations (c_0 and c_k , mol/dm³), the reaction rate constant (k) was calculated at different temperatures by non-linear regression according to the following (Eq. 2):

$$c_k = c_0 \cdot \exp(-k \cdot t) \quad (2)$$

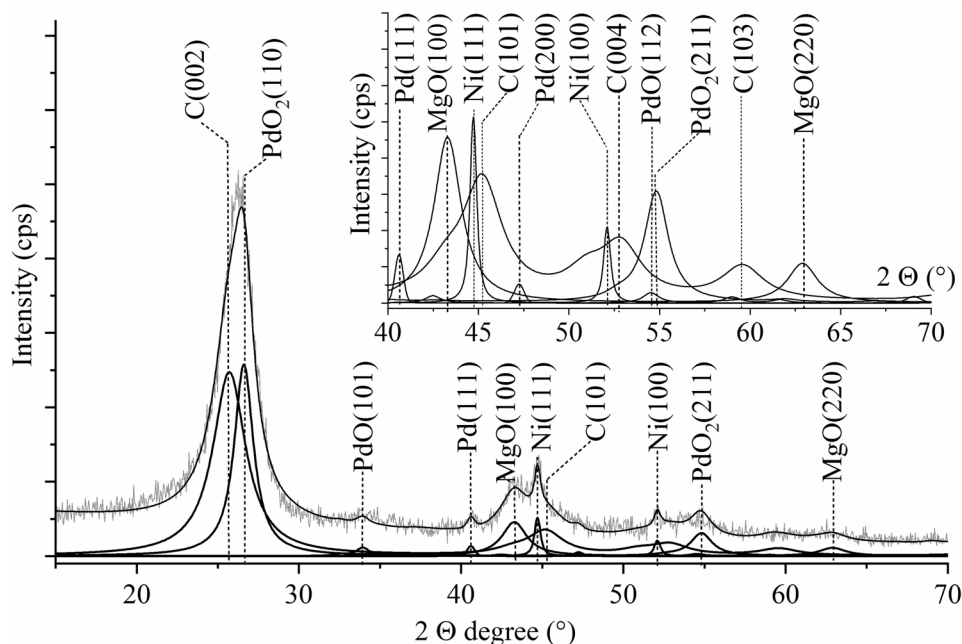
3 Results and Discussion

3.1 Characterization of the N-Doped Carbon Nanotube Supported Palladium Catalyst

The deconvoluted XRD pattern confirmed that the total amount of palladium nitrate has been reduced to palladium oxide (PdO and PdO₂) and elemental palladium (Fig. 1). The (101) and (112) reflexions of palladium(II) oxide have been identified at 33.3° and 53.7° two theta degrees on the diffractogram. The peaks at 27.2° and 54.7° two theta degrees were assigned to the (110) and (211) reflexions of the palladium(IV) oxide. The reflexions of the Pd(111) and Pd(200) are found in strong preferred orientation at 40.5° and 47.1° two theta degrees. The presence of elemental nickel and MgO have also been confirmed, which is due to the fact that nickel containing MgO catalyst was applied to synthesize the N-BCNT and in small quantities remained in the system afterwards.

The FTIR spectra of the pristine and the Pd decorated carbon nanotubes have been measured (Fig. 2). The absorbance at 1099 cm⁻¹ indicates the presence of incorporated nitrogen atoms. The stretching vibration mode of the C–O bonds is found at 1239 cm⁻¹. Peaks originated from the CNT structure can be found at 1631 cm⁻¹, 2897 cm⁻¹ and 2938 cm⁻¹ wavenumbers, which are corresponds to the C=C, and the symmetric and asymmetric C–H stretching vibrations, respectively. The band of the surface hydroxyl groups can be found at 3448 cm⁻¹, which includes the peaks of amine groups (νNH) as well.

Fig. 1 Deconvoluted XRD pattern of the synthesized Pd/N-BCNT catalyst



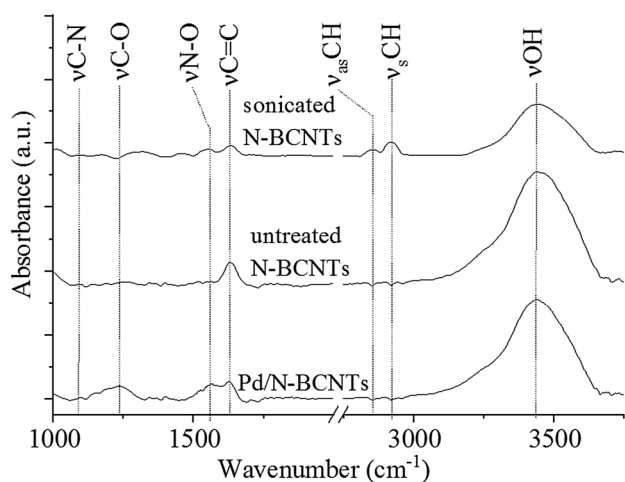
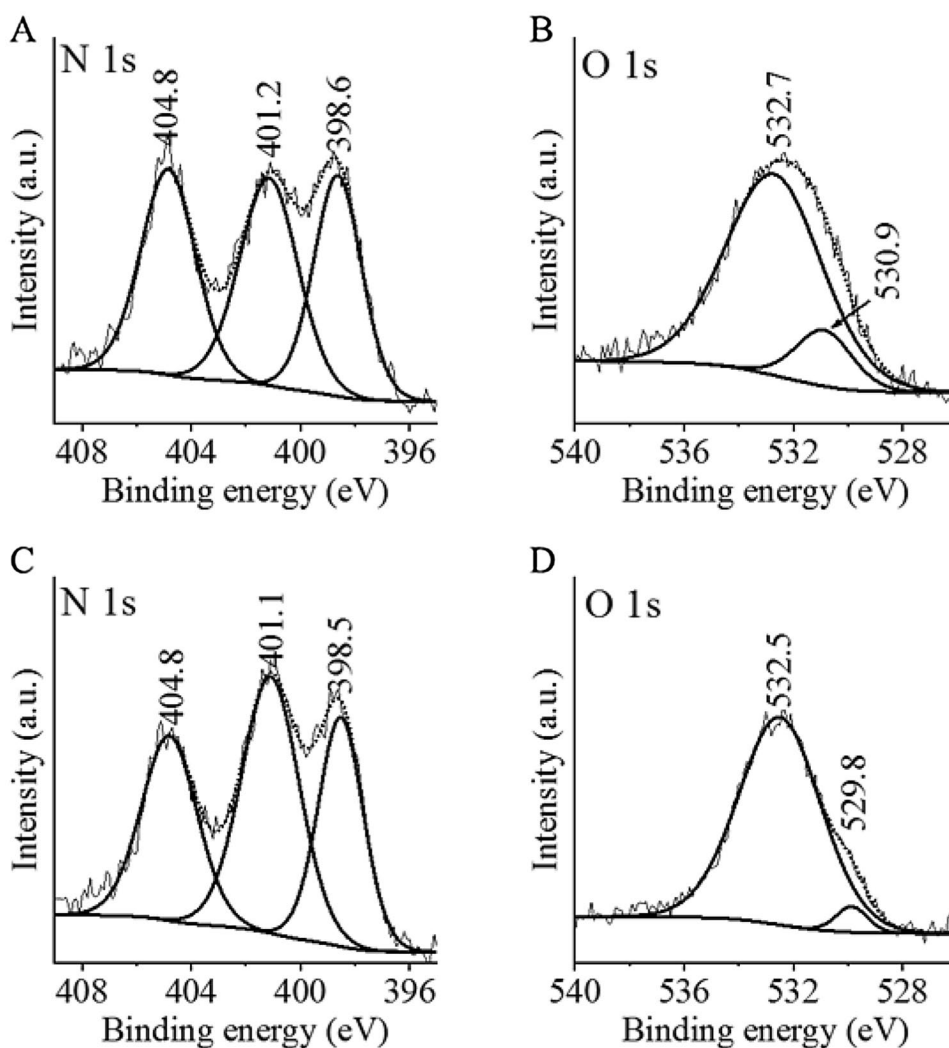


Fig. 2 FTIR spectra of sonicated and untreated N-BCNT and Pd/N-BCNT

The stretching vibration mode of the N–O bond only appeared in the spectrum of the Pd/N-BCNT sample (Fig. 2). The presence of νNO originated from the palladium precursor ($\text{Pd}(\text{NO}_3)_2$). During the reduction of palladium ions, carbon atoms were oxidized, which can be confirmed by the appearance of the intensive band at 1244 cm^{-1} which was identified as the $\nu\text{C-O}$ stretching. It can also be observed that the absorption band of the $-\text{COOH}$ groups around 1720 cm^{-1} cannot be found in the case of Pd/N-BCNT. Control experiment with N-BCNTs was carried out without the addition of Pd^{2+} ions under the same ultrasonic condition for comparison. The C–O band was not appeared in this case which means that, the oxidation of the N-BCNTs induced by the redox reaction which takes place between the palladium ions and nanotubes.

The N-BCNT samples were measured by XPS before and after the palladium decoration and the spectra are similar to each other regardless of the presence of Pd in the system. (Fig. 3). However, differences in the intensities of the peaks could be observed between the Pd free and Pd containing

Fig. 3 N1s band and O1s band of N-BCNT (a, b) and the Pd/N-BCNT catalyst (c, d), respectively



samples. On the deconvoluted N1s band three peaks were identified at 404.8 eV, 401.2 (401.1) eV and 398.6 (398.5) eV binding energy which are attributed to the oxidized pyridinic N atoms (pyridine oxide), quaternary and pyridinic nitrogen atoms, respectively (Fig. 3a, c). On the deconvoluted O1s band two peaks were located, the main peak can be attributed to the presence of surface hydroxides (Fig. 3b). In both cases a minor peak at lower binding energies was also observed which judging from its binding energy can be assigned to carbon-bound oxygen in the Pd free case and to palladium oxide in the decorated sample (Fig. 3d).

The ratio of the different nitrogen species has been changed by the Pd deposition (Table 1). The percentage of pyridinic N and the oxidized nitrogen species were decreased from 31.2 to 29.1% and 33.1 to 29.0% in case of the Pd/N-BCNT, respectively (Table 1). The decreased amount of pyridine N-oxide could be explained by a palladium catalysed deoxygenation process [32]. However, the percentage of the quaternary N increased from 35.7 to 41.9% after the Pd deposition.

Peaks are assigned to elemental palladium, PdO and PdO₂ in the XPS spectrum of the synthesized Pd/N-BCNT catalyst samples (Fig. 4). The presence of elemental palladium and

PdO have been indicated by two pair of bands at [340.7 eV, 332.2 eV] and [342.5 eV, 337.3 eV], respectively. However, these peaks are slightly shifted compare to the literature values, which can be explained by the small particle size in case of Pd (<5 nm) [33], and by the interaction with the catalyst support in case the PdO [34, 35]. Palladium(IV) oxide was also detected in the sample, and the corresponding bands are located at 343.6 eV and 338.4 eV binding energies.

The atomic percentage of the palladium forms were calculated with respect to the total palladium content of the Pd/N-BCNTs catalyst and it was found that 6.0% Pd and 47% PdO and 47% PdO₂ are present in the system. The total palladium content of the catalyst is 0.28% (atomic percentage), which is 2.5 wt% (percentage by weight). The C, N and O contents are not differ significantly between the samples (Table 2).

The palladium nanoparticles are smaller than 5 nm according to the HRTEM images (Fig. 5). The dispersibility of the Pd and PdO/PdO₂ nanoparticles is high.

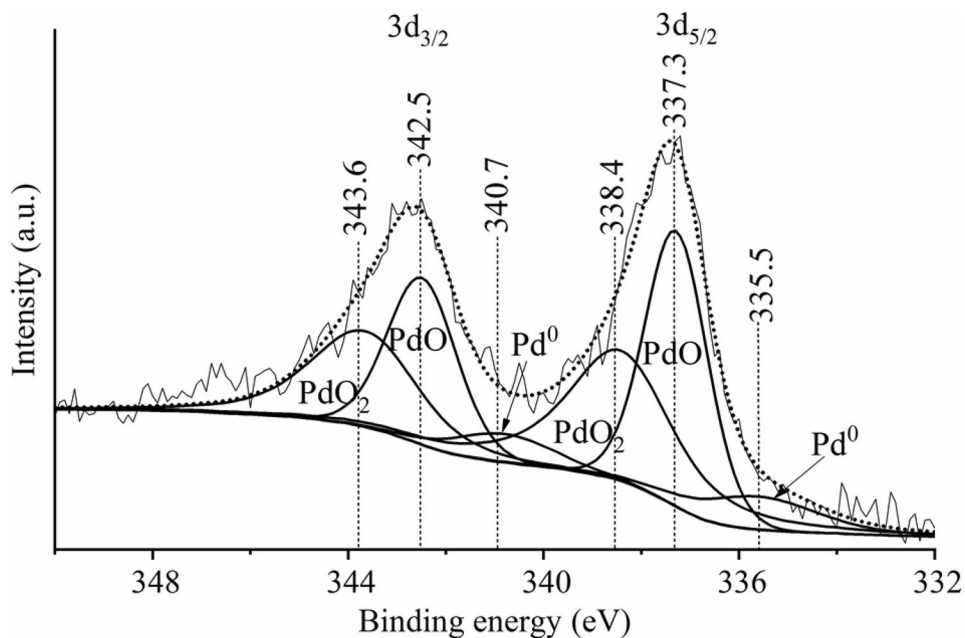
Table 1 Quantity of the different nitrogen forms in the N-BCNTs and the Pd/N-BCNTs

Sample	Atomic percentage of nitrogen (%)		
	Pyridinic N	Quaternary N	N-O _x species
N-BCNT	31.2	35.7	33.1
Pd/N-BCNT	29.1	41.9	29.0

Table 2 Atomic percentages of the elements in the N-BCNT and Pd/N-BCNT sample

Sample	Total Atomic percentage (%)			
	C1s	N1s	O1s	Pd 3d
N-BCNT	94.0	3.2	2.8	–
N-BCNT Pd	93.4	3.5	2.8	0.3

Fig. 4 Deconvoluted Pd 3d band of the Pd/N-BCNT catalyst



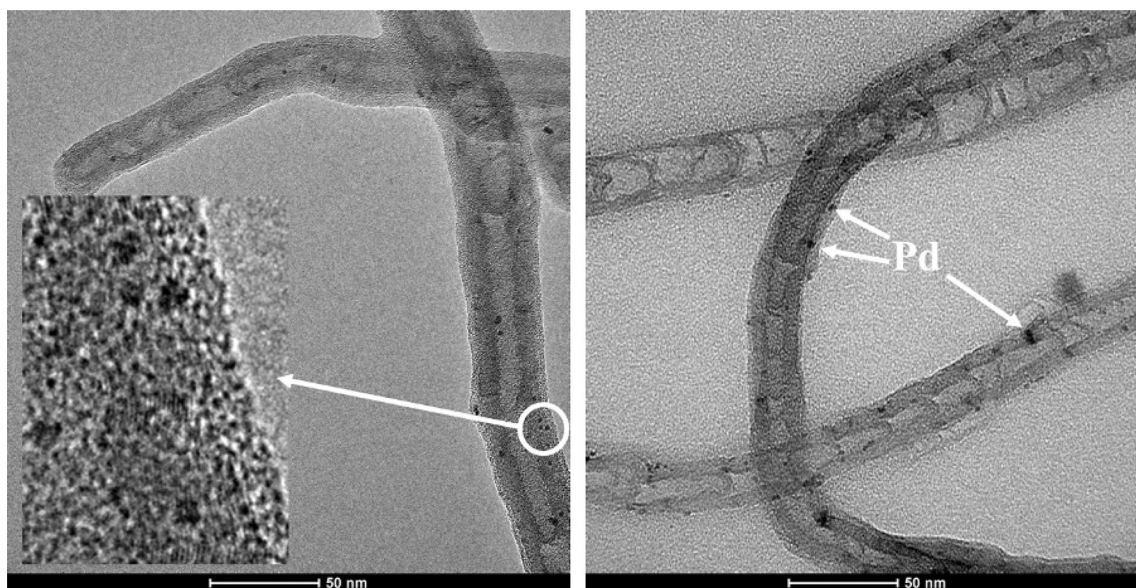


Fig. 5 HRTEM images of the Pd/N-BCNT catalyst

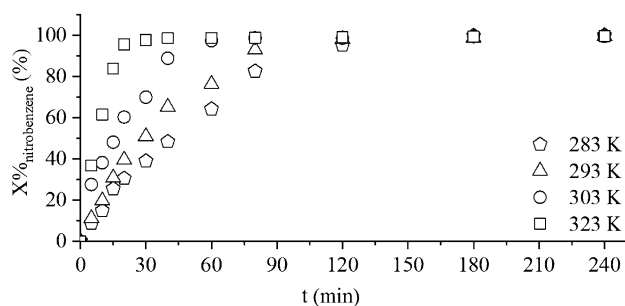


Fig. 6 Nitrobenzene conversion ($X\%$) vs time of hydrogenation

3.2 Catalytic Tests of the Pd/N-BCNT Catalyst in Nitrobenzene Hydrogenation

The synthesized Pd/N-BCNT catalyst was very efficient in each experiments, and the nitrobenzene conversion reached the maximum regardless the reaction temperature (Fig. 6). There is evidence in the literature, where the Pd oxide containing catalyst was more active, than the corresponding system which include only the metallic phase of palladium [36]. By increasing the reaction temperature, the reaction rate was also increased, at 323 K the conversion of nitrobenzene was 98.6%, while at 283 K the conversion was 48.3% after 40 min hydrogenation.

Intermediates (nitrosobenzene and azoxybenzene) and a by-product (*N*-methylaniline) have also been identified besides aniline (Fig. 7). The conversion of azoxybenzene to aniline is a fast process, which was detected only at lower temperatures (283 K and 293 K), where the reaction was

slower. The hydrogenation of nitrosobenzene intermediate to aniline was enhanced by increasing the reaction temperature. Only one by-product was formed at higher temperature (303 K and 323 K) values, *N*-methylaniline in a small concentration ($< 8 \text{ mmol/dm}^3$). By decreasing the reaction temperature, the reaction rate was also lower, but it was favourable for aniline selectivity and *N*-methylaniline was not formed.

Based on the nitrobenzene concentration of the samples, the reaction rate constants (k) at different temperatures were calculated (Table 3) by using a non-linear regression method (Fig. 8a) [37].

By applying the natural logarithm of reaction rate constants, the activation energy was also calculated using the Arrhenius plot. The (k) constants were plotted as a function of the temperature, and the activation energy can be calculated (Fig. 8b). The activation energy was 35.81 kJ/mol which is similar to other Pd, Pt or Ru containing catalysts [38–41].

4 Conclusion

A one-step catalyst preparation procedure has been successfully developed. A small fraction of palladium ions was reduced to Pd nanoparticles and deposited onto the surface of nitrogen-doped carbon nanotubes (N-BCNT) by acoustic cavitation using high-intensity ultrasound in aqueous phase, where N-BCNT served as a reducing agent. The overall procedure will lead to the deposition of elemental palladium, palladium(II) oxide and palladium(IV) oxide particles onto

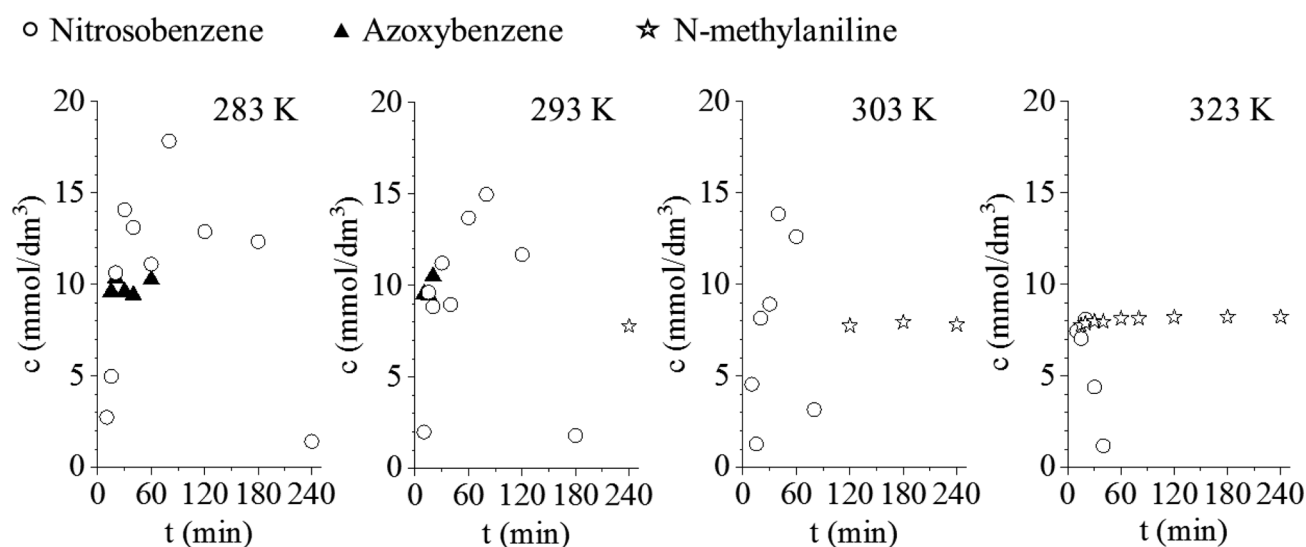


Fig. 7 Concentration of the intermediates and by-product vs time of hydrogenation at different temperature values

Table 3 Reaction rate constants at different temperatures

Temperature (K)	283	293	303	323
Reaction rate constant (s^{-1})	3.16×10^{-1}	4.35×10^{-1}	7.63×10^{-1}	1.84
SD	1.68×10^{-2}	1.67×10^{-2}	4.17×10^{-2}	1.07×10^{-1}

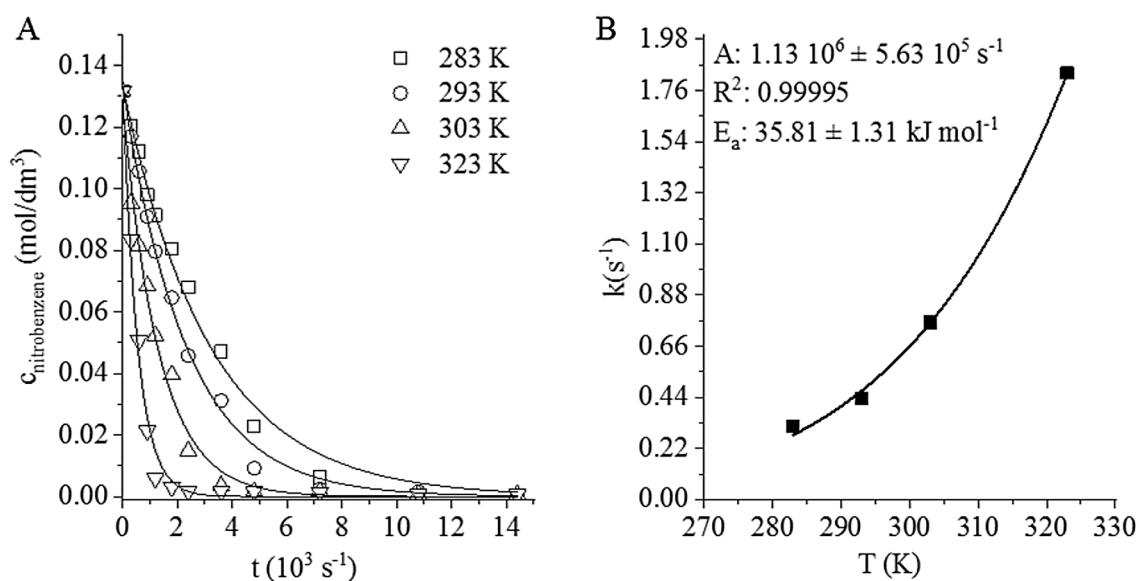


Fig. 8 Nitrobenzene concentration vs time of hydrogenation (a), and Arrhenius plot, k vs temperature (b)

the surface of the N-BCNT support. Thus, Pd/N-BCNT catalyst can be achieved in a one-step process.

Further activation was not necessary as the catalytic system was applicable in nitrobenzene hydrogenation. During the catalyst preparation, the N-BCNTs were oxidised and the formation of new oxygen containing groups confirmed

the oxidation process. The deposited palladium and palladium-oxide nanoparticles are smaller than 5 nm based on HRTEM pictures. Despite the high palladium-oxide ratio the synthesized Pd/N-BCNT catalyst was highly active in nitrobenzene hydrogenation as the conversion was 98% at 323 K after 40 min. Only one by-product (*N*-methylaniline)

in small quantities (8 mmol/dm³) was formed at higher temperature values. The activation energy was 35.81 kJ/mol, and it is similar to other works which indicates that the one-step procedure is applicable for catalyst preparation. All in all, the Pd/N-BCNT catalyst was successfully produced by using a one-step sonochemical method, where further activation was not necessary as the catalytic system was applicable in nitrobenzene hydrogenation.

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Compliance with Ethical Standards

Conflict of interest On behalf of all authors, the corresponding author states that there is no conflict of interest.

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