

1 Development of oral lyophilisates containing meloxicam 2 nanocrystals using QbD approach

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34 Abstract

35
36 The aim of this study was to develop oral lyophilisates with improved meloxicam (MEL)
37 dissolution, optimizing each step of the preparation by design of experiments. First, meloxicam
38 nanosuspensions were prepared by high-pressure homogenization (HPH), using PVP, Poloxamer
39 or PEG as stabilizers and were subjected to freeze-drying using mannitol as cryoprotectant. The
40 effects of the stabilizers and cryoprotectant were assessed and an optimal formulation was
41 generated within the design space where the particle sizes and the PDIs are at their lowest values.
42 The optimal formulation was used at the preparation of oral lyophilisates. Sodium alginate (SA)
43 and croscarmellose sodium (CCS) were tested as matrix forming agents and three different
44 freezing regimes were applied. The formulation was optimized, choosing the polymer that yielded

45 both high mechanical strength and fast MEL dissolution. Poloxamer led to particle size reduction
46 down to 10.27% of the initial size, meaning 477.6 ± 7.5 nm, with a slight increase during freeze-
47 drying process. PEG showed lower nanonizing capacity during HPH, but freeze-drying produced
48 further diminution of the particle size. Since Poloxamer provided advanced size reduction while
49 preserving MEL crystallinity, it was used for the optimized formulation containing 1% Poloxamer
50 and 5% mannitol added before freeze-drying. SA showed good structural properties when
51 compared to CCS and allowed fast MEL dissolution at low ratios. The optimal formulation
52 contained 1.157% of SA was subjected to thermal treatment during freeze-drying. It disintegrated
53 in 3.33 sec and released 77.14% of the MEL after 2 minutes. The quality by design (QbD) approach
54 for the development of pharmaceutical products ensured high quality of the dosage form and good
55 understanding of the preparation process.

56
57 **Keywords**

58 Nanocrystals, Meloxicam, Quality by Design, Oral lyophilisates, High-pressure homogenization

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62 **1. Introduction**

63 Oral solid dosage forms are preferred by patients for the accurate dosing, their stability, easy of
64 administration. Still, for the special groups of patients: pediatric, geriatric, patients with dysphagia,
65 their intake imposes serious limitations. The orally disintegrating dosage forms gained attention
66 from the pharmaceutical industry and academia for their numerous advantages: easy swallowing
67 without water, pleasant taste, enhancement of patent life cycle and increase of bioavailability of
68 poorly water soluble drugs (Al Husban et al., 2010, 2011).

69 In the case of orodispersible tablets (ODTs), bioavailability increases due to the quick
70 disintegration, followed by dissolution of the active pharmaceutical ingredient (API) in the saliva,
71 the direct absorption through the oral mucosa to the systemic circulation, bypassing the liver first-
72 pass metabolism (Al Husban et al., 2011). Fast disintegration occurs with highly porous products
73 obtained either by compressing at low compression forces, molding or by freeze-drying
74 (Chandrasekhar et al., 2009). Among these methods, freeze-drying provides light, porous
75 structures that disintegrate in a matter of seconds, “officially” known as oral lyophilisates.

76 When fast disintegration of the dosage form is granted, bioavailability can be further limited by
77 the API solubility and dissolution rate (Ghosh et al., 2012, Sarnes et al. 2014). To overcome this
78 issue, researchers developed solid dispersions, drug-cyclodextrin inclusion complexes and
79 nanosized particles (Samprasit et al., 2015, Blagden et al., 2007). Particle size reduction to the
80 nano range with the effective surface area increase showed promising results in terms of
81 dissolution rate and bioavailability improvement.

82 From the plethora of APIs being the subject of nanonization, meloxicam is a substance whose
83 action consists in the selective inhibition of cyclooxygenase-2 isoenzyme and therefore it has
84 effective anti-inflammatory and analgesic properties (Ochi et al., 2014) that recommend it for both
85 human and veterinary use (Monteiro et al., 2016). Besides that, it is also emerging as a promising
86 drug for the treatment of Alzheimer’s disease and cancer. It was categorized into class II of the
87 Biopharmaceutics Classification System (BCS), meaning it exhibits low water solubility (4.4
88 $\mu\text{g/ml}$) and good membrane permeability (Ambrus et al., 2009). Following the intake of classical

89 tablets, the peak plasma concentration is reached in 5-6 hours (Dellgado et al., 2014), far too long
90 for a quick onset of the effect, which motivates the development of a fast dispersible dosage form
91 with highly soluble meloxicam nanocrystals.

92 Nanocrystal technologies usually provide sub-micron colloidal dispersions of the drug crystals in
93 a solvent, which has to be eliminated to obtain the dry powder for the further preparation of a solid
94 dosage form (Kumar et al., 2015, Lai et al., 2015). One interesting approach is the combination of
95 nanosuspensions with the production of freeze-dried orodispersible tablets (Lai et al., 2011, 2014).
96 It involves the nanosuspension preparation and mixing with the matrix forming and cryoprotectant
97 excipients, followed by freeze-drying, thus obtaining the freeze-dried ODTs. However, the main
98 issues generated by the preparation of this new dosage form relate to the crystals' stability before,
99 after freeze-drying, and to the balance between the disintegration and structure resistance of the
100 freeze-dried products. The nanosuspensions are thermodynamically unstable systems, which can
101 be stabilized for a pharmaceutically relevant time by adding surfactants or polymers that act as
102 stabilizers. A high number of reports acknowledged the stability dependence on the type and
103 amount of stabilizer, but when freeze-drying process is involved, data about crystal aggregation
104 tendency is still controversial (Chung et al., 2012).

105 The design of a new formulation requires complete information about the process parameters and
106 the way they control the quality attributes. Optimization via empirical screening approach is time
107 consuming and does not reveal the collective effects of process and formulation factors. Design of
108 Experiments (DoE) method has been used to overcome these issues by offering a broad
109 understanding on the relationship between independent and dependent variables. Previous studies
110 reporting the development of oral lyophilisates containing nanocrystals (Lai et al., 2011, 2014)
111 used traditional screening approach and focused on API dissolution. They pointed out a complex
112 preparation process with numerous variables, each one having a potential impact on product
113 characteristics. Therefore, we believe that a research study conducted by a method that allows their
114 simultaneous study could add to the knowledge base valuable data.

115 In this study, a DoE approach was applied to understand and optimize the two important steps in
116 the preparation of oral lyophilisates (OLs) containing API nanocrystals: nanosuspension
117 preparation and oral lyophilisates preparation. MEL was used as a model drug due to its emerging
118 wide clinical applications and to the fact that such formulations of OLs containing MEL
119 nanoparticles have never been used. In the first step, we established the optimal stabilizer and the
120 mannitol ratios, after the evaluation of crystal behavior before and after freeze-drying. The second
121 step focused on the matrix forming agents' functions and on the freezing regime. We studied their
122 influence on the mechanical structure and the further on MEL dissolution.

123 The nanosuspensions were obtained by pre-sonication and high-pressure homogenization,
124 followed by freeze-drying that led to oral lyophilisates. The particle size, polydispersity index
125 (PDI) and Zeta potential were investigated as responses in the first step, while in the second
126 preparation step we evaluated the disintegration time, the texture analysis and the *in vitro* drug
127 release.

128

129 **2. Materials and methods**

130

131 2.1 Materials

132 The active pharmaceutical ingredient (API) – meloxicam (MEL) was purchased from Unichem
133 Laboratoires Ltd., India. Mannitol (M) (Pearlitol 200M) and polyethylene glycol 4000 (PEG 4000)

134 were purchased from Merck, Germany. PVP K25 (Kollidon 25) and Poloxamer 188 (Polox)
135 (Kolliphor P188) were kindly donated by BASF, Germany. Croscarmellose sodium (CCS) (Ac-
136 Di-Sol) was obtained from FMC BioPolymer, Belgium and the alginic acid sodium salt (SA) from
137 Sigma-Aldrich, United Kingdom.

138

139 2.2 Methods

140

141 2.2.1 Nanosuspension optimization

142 2.2.1.1 Design of experiment

143 Previous research in nanosuspension preparation revealed the importance of the stabilizer type and
144 concentration for the API dissolution behavior. The stabilizers should assure wetting of the
145 hydrophobic surfaces and increase of the activation energy of the agglomeration process, therefore
146 be a barrier to agglomeration (Van Eerdenbrugh et al., 2008). The **type of stabilizer** was set as
147 qualitative variable (X_1). We chose two polymers: PVP, PEG and one nonionic surfactant, Polox.
148 Their **weight concentrations** in volume were varied on three levels: 0.25 – 1 – 1.75% (w/V) (X_2).
149 During the freeze-drying, a cryoprotectant was added to avoid freeze damage due to ice formation
150 and particle aggregation (Wang et al. 2013). We chose mannitol as **cryoprotectant, at**
151 **concentrations** comprised between 0 and 5% (X_3). The effects of the aforementioned parameters
152 on the crystal size, polydispersity (PDI) and Zeta potential were investigated using a three-factor,
153 three-level DoE.

154 The critical quality attributes (CQAs) of the nanosuspensions were the average particle size and
155 the MEL crystallinity.

156 As responses, we chose the **particle size and PDI after the size reduction** (Y_1, Y_2) and
157 **after the freeze-drying** (Y_3, Y_4). In order to assess the size and PDI variations produced by freeze-
158 drying process only and test if they have any statistical significance within the DoE, we calculated
159 the size and PDI changes from the following equations:

160
$$\text{Size variation } (Y_5) = (\text{initial size} - \text{final size}) * 100 / \text{initial size}$$

161
$$\text{PDI variation } (Y_6) = (\text{initial PDI} - \text{final PDI}) * 100 / \text{initial PDI}.$$

162 The DoE modeling was performed using Modde 10.0 (Umetrics, Sweden) software and
163 was used to provide a surface model for the six mentioned responses and an optimized formulation
164 to take forward to the second step of the study.

165

166 2.2.1.2 Preparation of nanosuspensions

167 The micronized MEL (with $4.51 \pm 0.57 \mu\text{m}$ average size and polydispersity index equal to 1) was
168 suspended in the aqueous stabilizer (PVP, Polox or PEG) solution, using a magnetic stirrer to a
169 concentration of 0.75% (w/V). The suspensions were stirred for 10 minutes at 1000 rpm. Each of
170 them was then sonicated for 10 minutes at 70% amplitude using a high power ultrasound device
171 (Hielscher UP 200S Ultrasonic processor, Germany) to wet the drug. Further size reduction to
172 nanorange was achieved by applying high-pressure homogenization (HPH) with an Emulsiflex C5
173 apparatus (Avestin, Ottawa, Canada). 2 cycles at 500 bar were applied, followed by 20 cycles at
174 1000 bar.

175

176 2.2.1.3 Freeze-drying of nanosuspensions

177 MEL nanosuspensions were freeze-dried using a lab scale VirTis Advantage Plus freeze-drier (SP
178 Scientific, Gardiner, USA). Briefly, four 0.5ml samples were taken from each of the
179 nanosuspensions and poured into blister sockets. The blisters were placed on the freeze-dryer shelf
180 and cooled to -50°C at a rate of $1^\circ\text{C}/\text{minute}$, thus we applied a fast freezing regime. The

181 temperature was kept constant for 6 hours for complete product solidification. The primary drying
182 was performed at -20°C for 20 hours and vacuum of 0.2 mbar, followed by secondary drying at
183 5°C for 6 hours at 0.2 mbar.

184

185 *2.2.1.4 Particle size analysis*

186 Particle size measurements were performed by photon correlation spectroscopy (PCS) using a
187 Zetasizer Nano ZS90 (Malvern Instruments, UK). Both the nanosuspensions before freeze-drying
188 and the freeze-dried nanocrystals were subjected to this measurement. A mean particle diameter
189 at an angle of 90° and a constant temperature of 25°C and the width of the size distribution (PDI)
190 were determined by this method. 0.5ml of the suspension or corresponding freeze-dried product
191 were diluted to 15ml with purified water. All samples were subjected to 60s of sonication prior to
192 the size analysis in order to disperse the aggregates if present. Zeta potential was determined using
193 the same equipment, by estimating the particle electrophoretic mobility in a thermostated cell. The
194 results are presented as mean of three determinations and standard deviation.

195

196 *2.2.2. Oral lyophilisates optimization*

197 *2.2.2.1. Experimental design*

198 The optimal nanosuspension formulation revealed by the first DoE (containing 7.5 mg MEL/ml,
199 1% (w/V) Polox and 5% (w/V) mannitol) was taken forward to the next step, the formulation and
200 optimization of the oral lyophilisates. Once the nanosuspension characteristics were established,
201 we identified other factors that could influence the quality profile of the OLs: the type and content
202 of matrix forming agent and the freezing rate. The chosen matrix forming agents (**X₁**) were sodium
203 croscarmellose (**CCS**) at a ratio of **1%, 3% or 5%** and sodium alginate (**SA**) at a ratio of **1%, 2%**
204 **or 3%**. The matrix forming agent **percentages (X₂)** were chosen from viscosity studies (results
205 not shown); the viscosity had to be high enough to maintain suspension stability and still the
206 suspensions had to be fluid enough to be accurately poured into blister sockets. The CCS
207 percentages, of 1%, 3% and 5% were chosen from previous viscosity measurements that ranged
208 between 40 and 250 mPa s, while for the sodium alginate, the viscosities of the 1%, 2% and 3%
209 dispersions varied from 200 to 2000 mPa s. These dispersions were considered to be consistent
210 enough to maintain meloxicam stability before freezing, but still fluid enough to be accurately
211 poured into the blister sockets. The third independent variable was the **freezing type: fast, slow**
212 **or annealing (X₃)**.

213 The CQAs of OLs were the disintegration time, the mechanical strength and the MEL
214 dissolution profile.

215 Several evaluation methods were selected in order to monitor the CQAs and their results
216 were set as responses within the DoE. Therefore, we measured the **disintegration time (Y₁)**, the
217 **hardness (Y₂)**, the **fracturability (Y₃)**, the **% of dissolved MEL** after 2 minutes (**Y₄**), 4 minutes
218 (**Y₅**), 6 minutes (**Y₆**), 12 minutes (**Y₇**), 18 minutes (**Y₈**) and 30 minutes (**Y₉**).

219 The same software was used to test the model and obtain the optimized formulation.

220

221 *2.2.2.2. Preparation of oral lyophilisates*

222 The previously optimized nanosuspension (containing 7.5 mg MEL/ml, 1% (w/V) Polox and 5%
223 (w/V) mannitol) was prepared according to the described methods (2.2.1.2.). For each of the OL
224 formulations, the corresponding matrix forming agent was added in the indicated ratio and the

225 formed viscous suspension was kept under gentle stirring until the complete polymer dispersion
226 and homogenization.

227 0.5 ml of the obtained suspension that contained 3.75 mg MEL was poured into 30 blister sockets
228 (blister material: PVC-Aclar[®], PCTFE, poly-chloro-tri-fluoro-ethylene, cavity sizes: 12.70 mm
229 diameter x 5.50 mm depth) and freeze-dried (VirTis Advantage Plus, SP Scientific, Gardiner,
230 USA). The freeze-drying cycle started with one of the three proposed freezing profile (fast, slow
231 or annealing), followed by primary drying at -20°C for 20 hours and vacuum of 0.2 mbar and by
232 secondary drying at 5°C for 6 hours at 0.2 mbar (Fig. 1).

233

234 **Figure 1**

235

236 Fig. 2 illustrates the graphical procedure comprising the complete OL preparation process.

237

238 **Figure 2**

239

240 *2.2.2.3. Characterization of oral lyophilisates*

241

242 *The disintegration time* was measured according to Eur. Pharm. 8.0 method, by placing an oral
243 lyophilisate in 200ml distilled water kept at $20 \pm 0.5^\circ\text{C}$. The time necessary for complete
244 disintegration, until no solid residue was perceived, was recorded using a digital stopwatch. The
245 average disintegration time and the standard deviation of six tested tablets were calculated.

246

247 *The texture analysis* was performed using Brookfield TexturePro CT V1.5 (Brookfield
248 Engineering, USA). Tablets were extracted from the alveolae, placed on a horizontal rigid surface
249 and subjected to constant pressure. Pressure was applied by an acrylic probe (TA10), to a constant
250 deformation of 80%, at a test speed of 0.1mm/s and a load of 10 g. Load vs. distance curves were
251 recorded using Texture Pro Software. For each of the formulations, three measurements were
252 carried out for the average hardness at 1.6 mm, fracturability and their corresponding standard
253 deviations were calculated. The fracturability, as well as the hardness, derives from the texture
254 calculations. The analyzer measured the resistance of the sample to the advance of the acrylic
255 probe with a constant speed. The fracturability is calculated as the load value at the first fracture.
256 A fracture is a sudden load drop that indicates an abrupt resistance decrease in the sample. Low
257 fracturability values are correlated to brittle products. If no fracture occurs during the compression
258 cycle, the fracturability value equals the hardness value. The fracturability was determined for
259 three samples from each formulation; the mean value and the standard deviation were calculated.

260

261 *The in vitro dissolution test* was performed according to the Eur.Pharm. 8.0, using the paddle
262 method. 900 ml of phosphate buffer with pH 7.4 at 37°C were used as dissolution media, at a
263 rotating speed of 50 rpm. At certain time intervals, 5 ml samples were withdrawn, filtered through
264 0.2 μm cellulose filters (Phenomenex Syringe filters) and analyzed spectrophotometrically at 360
265 nm (Jasco V-560 UV-VIS, Easton, USA) against phosphate buffer pH 7.4 as a blank. Every sample
266 was replaced with the same volume of the fresh media. The experiment was done in triplicate and
267 the average meloxicam release at each sampling time and their standard deviations were
268 calculated.

269

270 *2.2.3. Solid state characterization of MEL nanocrystals*

271

272 2.2.3.1. X-ray powder diffraction (XRPD)

273 The physical state of MEL in the different stages of the preparation process (for raw MEL and the
274 freeze-dried nanosuspensions) was evaluated by XRPD. XRPD spectra were recorded with a
275 BRUKER D8 Advance X-ray diffractometer (Bruker AXS GmbH, Karlsruhe, Germany) system
276 with Cu K α 1 radiation ($\lambda = 1.5406 \text{ \AA}$) over the interval $5\text{-}30^\circ/2\theta$. The measurement conditions were
277 as follows: target, Cu; filter, Ni; voltage, 40 kV; current, 40 mA; time constant, 0.1 s; angular step
278 0.010. In the determination of the degree of crystallinity, the total area of the characteristic three
279 peaks with largest intensity was examined, after smoothing and background removal.

280

281 2.2.3.2. Scanning electron microscopy (SEM)

282 The morphology of the raw MEL, nanocrystals dried at room temperature without cryoprotectant
283 and freeze-dried products was examined by SEM (Hitachi S4700, Hitachi Scientific Ltd., Tokyo,
284 Japan). A sputter coating apparatus (Bio-Rad SC 502, VG Microtech, Uckfield, UK) was applied
285 to induce electric conductivity on the surface of the samples. The air pressure was 1.3-13.0 mPa.

286

287 3. Results and discussion

288

289 3.1. Optimization of nanosuspension

290 3.1.1. Experimental design

291 In order to achieve an optimal pharmaceutical product, all the possible variables that may influence
292 the characteristics of the product should be studied in detail. Two types of variables are involved
293 in the development procedure: formulation and process variables. In this study, we chose to focus
294 on the formulation parameters, while maintaining the process and its parameters at a constant level.
295 The preparation of nanosuspensions via high-pressure homogenization (HPH) offers a set of
296 advantages over the other size reduction methods, including low processing time, narrow size
297 distribution and few contamination sources (Wang et al., 2013). Moreover, the organic solvents
298 are not necessary, thus it is also ecologically friendly. Furthermore, HPH does not induce crystal
299 form transformation, which could relate to higher drug and dosage form stability (Wang et al.,
300 2013).

301 In this study, US preceded HPH, in order to disperse the eventual drug agglomerates and increase
302 the initial contact between the drug and the stabilizer. A constant number of HPH cycles was
303 chosen for each of the suspensions, at low pressure for the beginning and then at high pressure.

304 As stabilizers, we chose two polymers (PVP and PEG) and a nonionic surfactant (Polox). PVP
305 was previously used as an agglomeration inhibitor at the preparation of MEL microparticles and
306 nanocrystals (Pomazi et al., 2013, Bartos et al., 2015). In a grinding procedure to obtain MEL
307 nanocrystals, both PVP and PEG were used as stabilizers and were reported to significantly
308 improve the API dissolution rate (Kurti et al., 2011). Polox was confirmed as one of the most
309 efficient stabilizers with respect to the achieved size reduction, size distribution but also
310 concerning the morphology and aggregation capacity (Wang et al., 2013). Its high solubilizing
311 capacity was another reason for selecting it as excipient (Mata et al, 2005).

312 For the freeze-drying process, mannitol (M) was chosen as a cryoprotectant for its ability to dispose
313 between the nanocrystals in the cryoconcentrated product, to prevent aggregation and increase the
314 structure strength.

315 Based on preliminary experiments and literature data, the stabilizers (X_1), their ratios (X_2) and the
316 cryoprotectant (M) ratio (X_3) were set as critical factors. Thus, the study was conducted after a 3^3

317 factorial design for MEL nanosuspension formulation. To evaluate the nanosuspensions' behavior
318 through the preparation process and through freeze-drying, we chose to measure the size and PDI
319 after HPH (Y_1, Y_2), then after freeze-drying and reconstitution (Y_3, Y_4) and the size and PDI
320 variation caused by freeze-drying (Y_5, Y_6) (see Supplementary material, Table 1).

321

322 **Table 1**

323

324 Multiple linear regression analysis and ANOVA were used to develop a mathematical model for
325 each response. Equation 1 represents the general form of each model:

$$326 Y = B_0 + B_1X_1 + B_2X_2 + B_3X_3 + B_4X_1^2 + B_5X_2^2 + B_6X_3^2 + B_7X_1X_2 + B_8X_1X_3 + B_9X_3X_2 + B_{10}X_1X_2X_3$$

327 (eq.1),

328 where Y is the dependent variable (response), B_0 is the mean response (intercept) and B_i are
329 regression coefficients derived from the obtained experimental values. X_1, X_2, X_3 are individual
330 effects; they represent the result of the variation of one factor, while keeping the other factors at a
331 constant value. X_1^2, X_2^2 and X_3^2 are quadratic effects that indicate non-linear correlations with the
332 response. X_1X_2, X_3X_2, X_1X_3 and $X_1X_2X_3$ are interaction effects which reveal the variations of the
333 responses when 2 or more factors change simultaneously.

334 The revised values obtained for eq. 1 regression coefficients are listed in Table 1 for each of the
335 responses, together with their statistical significance, expressed as p -value. The coefficients
336 indicate the magnitude of the effect of each of the independent variables and the way in which the
337 factors influence the responses is given by + sign for positive influence, or – sign for negative
338 influence. It was observed that all chosen factors produced significant changes with the responses.
339 The regression coefficient R^2 was above 0.90 for responses Y_1, Y_2, Y_3 and Y_5 , 0.89 for Y_4 and 0.74
340 for Y_6 , which demonstrates the good fit of the data to the created model. When the size and PDI
341 were measured after HPH, the critical factors were the stabilizer type and ratio ($p < 0.05$). After
342 FD, the M ratio became the third critical factor. Two-way interactions between the type of
343 stabilizer /its concentration and after FD between the stabilizer concentration/ M ratio had a
344 significant influence on the nanocrystal size and PDI.

345

346 **Table 1**

347

348 *3.1.2. The average size and PDI after HPH (Y_1, Y_2)*

349 The average sizes after HPH ranged between 477.6 nm and 1232.0 nm, with PDIs between 0.29
350 and 0.88. The lowest particle size was met with the PVP and Polox, while the sizes reached after
351 the same procedure using PEG as a stabilizer led to high values up to 1.2 μm . The wide data
352 variations indicate the strong influence of the selected factors on the dependent variables. The
353 regression coefficients listed in Table 1 pointed out the way stabilizers influence the nanocrystal
354 formation. It seems that PVP caused the average size decrease, but the interactive effect between
355 the type of stabilizer and its ratio indicates the opposite, a positive effect on the size. The response
356 surface helps further understanding on this subject showing that up to 1.3 %, PVP generates MEL
357 size reduction, while upper ratios hold back the nanonization process. Similarly, the PDI decreased
358 up to 1% PVP and at higher concentrations it increased again. PEG produced the lowest size
359 decrease, down to a minimum of 854 nm. The high viscosity polymers create in the suspension
360 could be the reason for the impaired size reduction at high levels (Patel et al., 2014), due to the
361 homogenization process hindering. Polox caused the most abrupt size and PDI decrease and kept

362 its behavior even at high ratios, as indicated by the response surfaces in Fig.3. 1% Polox led to the
363 lowest crystal size of 477.6 nm and the corresponding PDI of 0.34.

364

365 *3.1.3. The average size and PDI after FD (Y_3 , Y_4)*

366 The size and the PDI after FD were measured to assess the influence of independent variables on
367 the global process. After HPH, M was dissolved in the obtained nanosuspensions, therefore its
368 effect became visible in the statistical data. The average particle sizes ranged between 489.5 nm
369 and 836.1 nm, so the upper limit decreased during FD. The results (Table 1) showed that PVP ratio
370 did not have a significant influence on the size, but its presence determined a high PDI. Polox
371 yielded low crystal sizes with no change of polydispersity degree (Fig. 3), while PEG determined
372 the lower size reduction and wide size distribution.

373 M displayed a significant negative effect on both average crystal size and PDI, because it prevented
374 aggregation in the cryoconcentrated system.

375

376 **Figure 3**

377

378 *3.1.4. The size and PDI variations caused by freeze-drying*

379 For a statistical evaluation of the crystal size and PDI variations induced selectively by the freeze-
380 drying process, we calculated the percentages of size and PDI increase/decrease and tested them
381 as responses in the experimental design (see Supplementary material, Table 1).

382 Apparently, for most of the freeze-dried nanosuspensions, the crystal size decreased (14 out of 19).
383 The regression coefficients indicate which of the formulation factors influence the variation and
384 how (Table 1). An individual positive effect for PVP as stabilizer was obtained, meaning that at
385 low concentrations, PVP determined the size increase during FD. If the PVP ratio is too low, it is
386 possible that it does not cover the entire particle surface by adsorption (Wang et al., 2013).
387 Therefore, the uncovered sides of MEL particles could exhibit aggregation capacity and lead to
388 average size increase. An interactive negative effect between PVP as stabilizer and the stabilizer
389 concentration showed that high PVP content led to size reduction during FD, which confirms the
390 previous hypothesis. According to the statistical data, Polox had a positive effect on crystal sizes,
391 along the entire concentration range. On the opposite, freeze-drying nanosuspensions with PEG as
392 stabilizer determined a significant particle size decrease. ~~As PEG is highly hydrophilic, it could
393 adsorb water by hydrogen bonding and the freezing water molecules could break the stabilized
394 conglomerates into smaller particles.~~

395 M was added to the system when size reduction process was finished, therefore we expected it to
396 prevent aggregation and not to decrease the average size below the initial values. Surprisingly, the
397 sizes decreased even further. The explanation could be that M solution penetrated into the particle
398 fissures and when M crystallized during FD, the volume increase generated cracks into the crystal
399 aggregates with consequent size reduction.

400

401 *3.1.5. The Zeta potential*

402 The Zeta potential is a parameter that indicates the stability of nanosuspensions with values
403 between -100 mV and 100 mV. Products with Zeta potentials in the range [-25mV; 25mV] are
404 considered less stable, with high agglomeration probability. The values we obtained after HPH
405 ranged between -35.6 mV and -20.1 mV and suggest good stability for most of the
406 nanosuspensions (results not shown).

407

408 *3.1.6. Solid state characterization of MEL nanocrystals*

409
410 *SEM analysis*
411 The SEM images with reduced size MEL containing the same amount of stabilizer (1%), showed
412 the changes in the appearance and morphology of the obtained nanoparticles (Fig. 4). The large
413 raw MEL crystals (A) presented regular prismatic shape with smooth surfaces. The particle size
414 reduced, regardless of the type of stabilizer (B-D). PVP softened and covered the MEL particles
415 (Martha et al., 2013) that kept their shapes within an amorphous conglomerate (B). The
416 aggregation tendency of the MEL-PVP particles is visible in the SEM captions.
417 Polox as stabilizer led to oval shaped individual crystals (C) with soft edges that could be attributed
418 to erosion phenomena during the homogenization process. Partial dissolution of Mel crystals
419 mediated by Polox could also be incriminated, but since Polox critical micelle concentration is
420 higher than the ones used in our study (between 24 and 32 mg/ml according to Moghimi et al.,
421 2004), mechanical softening of crystal edges is more probable. The analyzed sample showed good
422 size uniformity, also confirmed by PCS.
423 PEG particles preserved their sharp edges, but they had a wide size distribution and the size
424 reduction did not reach the level of the other two stabilizers.

425 426 **Figure 4**

427 428 *XRPD analysis*

429 X-ray powder diffraction was performed for raw MEL and the freeze-dried nanosuspensions
430 prepared according to the experimental design. It was meant to assess the crystalline changes that
431 MEL might have suffered during the HPH and freeze-drying processes. The diffractogram of raw
432 MEL exhibits numerous distinct peaks, at diffraction angles 2θ of 13.22, 15.06 and 26.46 (Kurti
433 et al., 2011), which confirm its initial crystallinity. Fig. 5 shows the diffractograms of the freeze-
434 dried nanosuspensions and the changes that appear with different types and ratios of stabilizers.
435 For the sample with low PVP content (N8), the MEL characteristic peaks can be observed, but at
436 high PVP ratios the areas under the peaks considerably diminished (N11, N13), revealing the
437 amorphous structure of the nanoparticles. The products samples containing Polox as stabilizer
438 displayed all the MEL characteristic peaks at all concentration levels of the stabilizer, which
439 indicates that the crystalline state was preserved (N9, N12, N13). The PEG freeze-dried
440 nanosuspensions exhibited partial loss of crystallinity at low PEG concentrations (N15) (Martha
441 et al., 2013).

442 443 **Figure 5**

444 445 *3.1.7. Optimization of nanosuspension*

446 Based on the revised equations and surface response plots, the software was used to generate the
447 set of conditions/ optimum formulation variables in order to obtain the nanosuspensions with
448 desired CQA profile. The selected criterions were to minimize the average sizes and PDI after
449 HPH and after freeze-drying and to have a crystalline product. The software generated the
450 following conditions: Polox as stabilizer at 1% ratio and 5% M as cryoprotectant during freeze-
451 drying. Through statistical analysis, from the initial experimental area, a Design Space was
452 identified (Figure 6), where all the conditions imposed to the nanosuspensions formulations would
453 be fulfilled at a specified risk level. Each point from the Design Space represents a nanosuspension
454 formulation obtained with a risk level expressed as Defect per one Million Opportunities (DPMO).
455 The green areas could deliver a series of formulations that would comply to the conditions of low

456 average size and PDI, with a probability of 99.95%. The optimal nanosuspension was obtained
457 using the indicated parameters and the same procedure: the US, HPH and freeze-drying regimes
458 applied during the initial experiments. It exhibited a Zeta potential of -28.31 ± 0.48 mV, therefore
459 good stability. The characterization of the optimal formulation compared to the predicted values
460 and the calculated residuals are presented in Table 2. The closeness between the experimental and
461 the predicted results confirmed the validity of the statistical model and its predictive power. The
462 optimal suspension evaluated in Table 2 contains 7.5 mg MEL/ml, 1% (w/V) Polox 188 and 5%
463 (w/V) M.

464

465 **Figure 6**

466

467 **Table 2**

468

469

470 *3.2. Optimization of oral lyophilisates*

471

472 *3.2.1. Design of experiment*

473 The optimal nanosuspension was taken forward to the next step, an experimental design for the
474 optimization of oral lyophilisates. At this stage, the CQAs are disintegration time, mechanical
475 strength and MEL dissolution which is granted by the size reduction achieved in the first step
476 (Mauludin et al., 2009). A thorough study of the formulation factors is necessary in order to
477 balance the quick disintegration time and the high mechanical strength. Both disintegration time
478 and mechanical strength are conditioned by the type and ratio of matrix forming agents, while the
479 structure depends on the freezing rate (Harnkarnsujarit et al., 2012).

480 As matrix forming agents we chose CCS, superdisintegrant used for its high hydrating and swelling
481 capacity that grants suspension stability up to the freezing step. Moreover, it was mentioned for
482 the ability to increase API dissolution (Lai et al., 2014). SA was selected for its capacity to yield
483 highly viscous dispersions at low polymer concentrations (Vicini et al., 2015). The concentration
484 levels were chosen from previous viscosity studies (results not shown) so that the dispersions
485 would be fluid enough to be poured into blister sockets and viscous enough to prevent settling
486 phenomena: 1-3-5% for CCS and 1-2-3% for SA.

487 During the lyophilization process, the freezing step is of high importance due to the crystallization
488 processes that further impact the texture of the frozen matrix and the morphological characteristics
489 of the dried cake. For orally disintegrating dosage forms, slow freezing is more appropriate due to
490 the formation of structures with large pores, easily disintegrating upon hydration. Large pores
491 promote disintegration, but when it comes to systems containing suspended nanocrystals, a dense
492 cryoconcentrated phase during freezing could induce aggregation phenomena. Therefore, we
493 planned to study the influence of two different freezing rates: 0.5°/minute decrease (slow freezing),
494 1°/minute decrease (fast freezing) (Fig. 1). An annealing step was also considered for its reported
495 benefits on size distribution of ice crystals, on accelerating primary drying and reducing
496 heterogeneity between samples (Abdelwahed et al., 2006). Moreover, mannitol as bulking agent
497 is known to yield a mixture of amorphous and crystalline forms (Kim et al. 1998, Torrado et al.,
498 2002) especially at low mannitol ratios, therefore an annealing step integrated into the freezing
499 phase could maximize its crystallization (Mehta et al., 2013). The aforementioned independent
500 variables were included in a quadratic D-Optimal design: the type of matrix forming agent (X_1),
501 the matrix forming agent ratio (X_2) and the freezing rate (X_3). As responses, we chose the
502 disintegration time (Y_1), the hardness (Y_2), the fracturability (Y_3) and the percentage of dissolved

503 MEL at 2 minutes (Y₄), 4 minutes (Y₅), 6 minutes (Y₆), 12 minutes (Y₇), 18 minutes (Y₈) and 30
504 minutes (Y₉). For the evaluation of the results (listed in Supplementary material, Table 2), multiple
505 linear regression and ANOVA test were applied. They showed high variability, which indicates a
506 strong dependence on the selected independent factors. A model was developed for each response,
507 expressed as an equation of the response as a function of the independent variables and their
508 interactions (eq. 1, 3.1.1.).

509 The statistical analysis showed that all the selected independent variables had a significant
510 influence on the responses. R² was above 0.9 for responses Y₁, Y₃, Y₄, Y₅ and Y₆ and between 0.8
511 and 0.9 for Y₂, Y₇, Y₈ and Y₉, meaning that more than 80% of the responses variability was
512 explained by the model.

513

514 **Table 4**

515

516 *3.2.2. The disintegration time (Y₁)*

517 The OLs disintegrated between 0.83 and 58 s, ~~as shown in Table 4~~. The results proved that the
518 type of matrix forming agent (X₁), its ratio (X₂) and the freezing rate (X₃) significantly influenced
519 the disintegration time (Fig. 7). As expected, high CCS content determined a fast disintegration,
520 while high SA percentages led to slowly disintegrating OLs. The type of freezing also influenced
521 the disintegration: annealing decreased the disintegration time, while progressive freezing delayed
522 it. An interactive effect was noticed between the matrix forming agent (MFA) content and the type
523 of freezing: when annealing, the higher the MFA content, lower the disintegration time. On the
524 contrary, if progressive freezing was applied on highly concentrated MFA dispersions,
525 disintegration was delayed. Disintegration depends on the structure of the 3D freeze-dried matrix.
526 Annealing procedure allows the rearrangement of crystals with the structure relaxation; therefore,
527 it usually leads to highly porous products, easily permeated by the dissolution media.

528

529 **Figure 7**

530

531 *3.2.3. The texture analysis*

532 The OLs were completely dry freeze-dried matrices, with the diameter of 12.75 ± 0.15 mm and
533 the height of 5.14 ± 0.18 mm. The texture analysis revealed the OL's behavior when being
534 subjected to constant pressure. It yielded two parameters: the hardness (Y₂) and the fracturability
535 (Y₃), which describe the mechanical properties of the structures. The two MFAs yielded quite
536 different products. The OLs with CCS were extremely soft and fragile, while the OLs containing
537 SA gave firm and stiff structures, easy to extract from the blister sockets. Therefore, the only
538 significant influence was assessed with the MFA variation: CCS determined hardness decrease,
539 while SA determined the hardness increase, with no significant influence from their ratios (Fig.8
540 A).

541 Fracturability is an indirect indicator of the brittleness of a product and is calculated as the load
542 value at the first fracture, more precisely, it shows the resistance of a product to fractures. The
543 influence of the MFAs was, as expected, the most important: SA gave high fracturability, while
544 CCS gave low fracturability and their ratio increase determined higher fracture resistance in both
545 cases (Fig. 8B).

546

547 **Figure 8**

548

549 The mechanical profile of the oral lyophilisates was represented as load (N) vs. distance (mm)
550 curves (Fig. 9) and clearly shows the differences between CCS and SA behavior as structural
551 excipients. The weak CCS matrix appears like a very heterogeneous porous structure with thin,
552 disrupted pore walls. As for the suspensions containing SA, the dehydration led to a highly porous
553 structure, with big cavities produced by water crystals sublimation, but with slightly thicker pore
554 walls, linked to each other.

555

556 **Figure 9**

557

558 Interestingly, the type of freezing had no significant effect on the product's hardness or
559 fracturability parameters (Fig. 8) when analyzed within the experimental design, but a closer
560 texture curve analysis (results not shown) shows that progressive freezing yields weak mechanical
561 profiles as compared to the other freezing treatments.

562

563 *3.2.4. In vitro dissolution test*

564 The drug release from the lyophilized matrix was assessed by *in vitro* dissolution studies.
565 Dissolution is a limiting factor for the oral absorption and thus for the pharmacological effect. In
566 this study, the dissolution profiles were studied on a 30 minutes range, in PBS pH 7.4.

567 After 2 minutes, the ratio of dissolved MEL ranged between 21.57% and 100%. The wide range
568 shows the strong influence of independent variables on the responses. The influences of
569 independent variables on the dissolution profile were constant at all the tested times. MEL
570 dissolution was favored by the presence of CCS and delayed by SA. The higher the CCS ratio,
571 more MEL was dissolved. On the contrary, at high SA ratios, the dissolution percentages
572 decreased. The freezing rate influenced the dissolution profile during the first 6 minutes of the test;
573 after 6 minutes, more than 90% of MEL was dissolved for 15 formulations out of 21.

574 The sudden freezing delayed the dissolution, while the progressive freezing and the annealing
575 seemed to have a less significant enhancing effect on dissolution. The faster dissolution caused by
576 slow freezing could be a consequence of the weak mechanical strength it delivers and the higher
577 porosity produced by ice crystal growth in the freezing phase (Iurian et al., 2016).

578

579 **Figure 10**

580

581 *3.2.5. Optimization of oral lyophilisates*

582 The statistical calculations and experimental observations led to an accurate knowledge of the
583 variables that influence OL's characteristics. MEL dissolution was granted by its size reduction,
584 while the OL's disintegration and mechanical properties were controlled by the MFA type and
585 ratio and by the freezing regime. The statistics software was used to generate the optimal OL
586 formulation, by applying a set of constraints. We chose to minimize the disintegration time and
587 maximize the mechanical strength and MEL dissolution after 2, 4 and 6 minutes. The software
588 indicated the optimal formulation with SA as MFA, at -0.843 concentration level, meaning 1.157%
589 SA and being subjected to annealing as a thermal treatment before freeze-drying.

590 The optimal OLs were prepared and tested following the same techniques as the previous
591 formulations using the independent variables that resulted from the experimental design analysis.
592 The optimal formulation characterization is listed in Table 3. All the responses were in the
593 predicted range, therefore the experimental design was considered valid and could be further used
594 for the development of oral lyophilisates with desired characteristics.

595 **Table 3**

596 **4. Conclusion**

597 The study reveals a two steps QbD strategy for the development of oral lyophilisates with high
598 drug bioavailability. The first stage handles the development of an optimal nanosuspension with
599 respect to the crystal size and PDI, with focus on the changes brought by freeze-drying process
600 and how do different factors influence those changes. The optimal formulation that achieved the
601 lowest average size and PDI both before and after freeze-drying contained 1% Polox as stabilizer
602 and was submitted to lyophilization having 5% M as cryoprotectant. It was included in the second
603 step of the study for oral lyophilisates optimization, when three more variables were added: the
604 matrix forming agent type, ratio and the freezing regime. Sodium alginate granted high structural
605 stability but also fast disintegration and drug dissolution, therefore it was selected as matrix
606 forming agent in the optimal formulation.

607 The experimental design approach was a valuable tool for the thorough study of variables
608 influencing the nanosuspension and oral lyophilisate preparation. Creating such models offers high
609 versatility; the two validated experimental designs could be further used together for the
610 preparation of oral lyophilisates or separately as basis for other research studies. The optimal oral
611 lyophilisates according to Table 3 contain: 3.75 mg MEL/OL, 5 mg Polox 188/OL, 25 mg
612 mannitol/OL and 5.78 mg Sodium Alginate/OL, obtained from the freeze-drying a suspension that
613 contained 7.5 mg MEL/ml, 1% (w/V) Polox 188, 5% (w/V) mannitol and 1,157% (w/V) sodium
614 alginate.

615

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Table 1

The revised quantitative factor effects and associated *p* values for the responses

Term	Size after HPH (Y ₁)	PDI after HPH (Y ₂)	Size after FD (Y ₃)	PDI after FD (Y ₄)	Size variation after FD (Y ₅)	PDI variation after FD (Y ₆)
Constant	681.437 (0.000)	-0.429 (0.000)	2.770 (0.000)	-0.472 (0.000)	-11.168 (0.000)	-41.753 (0.000)
X ₁ PVP	-76.058 (0.000)	-0.071 (0.000)	-0.007 (0.471)	0.031 (0.087)	5.329 (0.002)	7.205 (0.000)
X ₁ Poloxamer	-138.297 (0.000)	-0.059 (0.000)	-0.037 (0.002)	-0.072 (0.000)	8.854 (0.000)	-0.344 (0.000)
X ₁ PEG	214.355 (0.000)	0.130 (0.000)	0.044 (0.001)	0.040 (0.037)	-14.184 (0.000)	-6.860 (0.000)
X ₂	106.637 (0.000)	0.058 (0.000)	0.005 (0.593)	-0.062 (0.006)	-9.267 (0.000)	-6.906 (0.000)
X ₃	3.470 (0.804)	-0.000 (0.916)	-0.025 (0.008)	-0.008 (0.102)	-4.603 (0.002)	-2.035 (0.002)
X ₂ *X ₂	90.858 (0.017)	0.129 (0.000)	0.037 (0.068)	-	-	7.695 (0.000)
X ₁ PVP*X ₂	54.710 (0.007)	-0.008 (0.375)	0.019 (0.072)	-	-7.576 (0.000)	-
X ₁ Poloxamer *X ₂	-114.159 (0.000)	-0.027 (0.012)	-0.048 (0.000)	-	4.927 (0.005)	-
X ₁ PEG *X ₂	59.449 (0.004)	0.035 (0.008)	0.029 (0.010)	-	2.649 (0.088)	-
X ₂ *X ₃	-	-	0.026 (0.007)	0.057 (0.003)	5.574 (0.000)	7.658 (0.002)
X ₃ *X ₃	-	-	-	-	-	-4.595 (0.000)

Table 2
Optimal nanosuspension formulation results

	Experimental values	Predicted values	Residual
Size after HPH (nm)	463.5 ± 9.71	453	10.5
PDI after HPH	0.312 ± 0.014	0.302	0.01
Size after Freeze-drying (nm)	501.7 ± 9.18	491	10.7
PDI after Freeze-drying	0.301 ± 0.037	0.291	0.01

Table 3
Optimal oral lyophilisate formulation results

	Experimental values	Predicted values	Residual
Disintegration time (s)	3.33 ± 0.76	1.89	1.44
Hardness (N)	16.34 ± 0.48	16.10	0.24
Fracturability (N)	22.58 ± 4.36	21.19	1.38
% of dissolved Mel after 2 minutes	77.14 ± 6.55	71.79	5.34
% of dissolved Mel after 4 minutes	86.82 ± 8.64	93.77	-6.95
% of dissolved Mel after 6 minutes	96.71 ± 4.11	100.41	-3.70